## Handout 14

## Chemical potential

## Definition

The chemical potential controls the flow of particles between different parts of a system, just like temperature controls the flow of heat. It is defined by

$$
\begin{equation*}
\mu=-T\left(\frac{\partial S}{\partial N}\right)_{U, V} \tag{1}
\end{equation*}
$$

In lectures, we considered a $p V$ system made up of two parts in contact such that the two parts can exchange internal energy, volume and particles. We applied the entropy maximum statement of the Second Law to show that, in equilibrium,

$$
\begin{align*}
\left(\frac{\partial S_{1}}{\partial U_{1}}\right)_{V, N} & =\left(\frac{\partial S_{2}}{\partial U_{2}}\right)_{V, N} \\
\left(\frac{\partial S_{1}}{\partial V_{1}}\right)_{U, N} & =\left(\frac{\partial S_{2}}{\partial V_{2}}\right)_{U, N} \\
\left(\frac{\partial S_{1}}{\partial N_{1}}\right)_{U, V} & =\left(\frac{\partial S_{2}}{\partial N_{2}}\right)_{U, V} \tag{2}
\end{align*}
$$

From the definitions of $T, p$ and $\mu$ [the latter in eqn. (1)], these conditions may be expressed

$$
T_{1}=T_{2}, \quad p_{1}=p_{2}, \quad \mu_{1}=\mu_{2} .
$$

## Thermodynamic potentials

With a variable number of particles of a single type, the fundamental eq. takes the form

$$
\begin{equation*}
\mathrm{d} U=T \mathrm{~d} S-p \mathrm{~d} V+\mu \mathrm{d} N \tag{3}
\end{equation*}
$$

The Helmholtz and Gibbs functions follow:

$$
\begin{align*}
\mathrm{d} F & =-S \mathrm{~d} T-p \mathrm{~d} V+\mu \mathrm{d} N  \tag{4}\\
\mathrm{~d} G & =-S \mathrm{~d} T+V \mathrm{~d} p+\mu \mathrm{d} N . \tag{5}
\end{align*}
$$

Hence,

$$
\begin{equation*}
\mu=\left(\frac{\partial F}{\partial N}\right)_{T, V}=\left(\frac{\partial G}{\partial N}\right)_{p, T} \tag{6}
\end{equation*}
$$

$G$ is extensive and may be written $G=N g(p, T)$. Therefore, from (6),

$$
\begin{equation*}
G=\mu N . \tag{7}
\end{equation*}
$$

If more than one type of particle is present, eqs. (3)-(7) generalise to

$$
\begin{equation*}
\mathrm{d} U=T \mathrm{~d} S-p \mathrm{~d} V+\sum_{i} \mu_{i} \mathrm{~d} N_{i} \text { etc, and } \quad G=\sum_{i} \mu_{i} N_{i} \tag{8}
\end{equation*}
$$

## Gibbs-Duhem equation

Differentiating (7) and equating to (5), we obtain

$$
\begin{equation*}
\mathrm{d} \mu=-s \mathrm{~d} T+v \mathrm{~d} p, \tag{9}
\end{equation*}
$$

where $s=S / N$ and $v=V / N$ are the entropy and volume per particle, respectively. Eqn. (9) relates the intensive variables of a system and is known as the Gibbs-Duhem equation. The generalisation to many components is

$$
\begin{equation*}
\sum_{i} x_{i} \mathrm{~d} \mu_{i}=-s \mathrm{~d} T+v \mathrm{~d} p, \tag{10}
\end{equation*}
$$

where $x_{i}=N_{i} / N$.

## Phase equilibrium

It can be shown that for a two-component system, equilibrium is reached when $\mu_{1}=\mu_{2}$. This is true for any constraints imposed on the system. Consider the phase boundary in the $p-T$ plane for a discontinuous phase transition, e.g. liquid-vapour or solid-liquid. All along the phase boundary $\mu_{1}=\mu_{2}$, so if two nearby points on the phase boundary are separated by intervals $\mathrm{d} p$ and $\mathrm{d} T$, then $\mathrm{d} \mu_{1}=\mathrm{d} \mu_{2}$. Therefore, from (9),

$$
\begin{equation*}
\frac{\mathrm{d} p}{\mathrm{~d} T}=\frac{s_{2}-s_{1}}{v_{2}-v_{1}}=\frac{L}{T \Delta V} . \tag{11}
\end{equation*}
$$

This is the Clausius-Clapeyron equation. Here, $L=T \Delta S$ is the latent heat. Note that $L$ and $\Delta V$ must both be normalised consistently, e.g. both per mole, or both per unit mass.

The Clausius-Clapeyron equation can be integrated to obtain the equation of the phase boundary in the $p-T$ plane. For the liquid-vapour phase boundary the result is

$$
\begin{equation*}
p \approx p_{0} \mathrm{e}^{-\frac{L}{R T}} \tag{12}
\end{equation*}
$$

assuming $L$ is a constant and $p V_{\text {vap }}=R T$. On the liquid-solid phase boundary the result is

$$
\begin{equation*}
p \approx p_{0}+\frac{L}{\Delta V} \ln \left(\frac{T}{T_{0}}\right) \tag{13}
\end{equation*}
$$

assuming $L$ and $\Delta V$ are constant.
In general, $L$ is only approximately constant. For the liquid-vapour phase boundary, the temperature dependence of $L$ is approximately

$$
\begin{equation*}
L(T)=\Delta C_{p} T+L_{0} \tag{14}
\end{equation*}
$$

where $\Delta C_{p}=C_{p_{\text {vap }}}-C_{p_{\text {liq }}}$. Equation (14) follows from eqn. (11) assuming (i) that the vapour is an ideal gas, (ii) that $V_{\text {vap }} \gg V_{\text {liq }}$, and (iii) that the heat capacities of the two phases are independent of temperature. $\Delta C_{p}$ would usually be negative since $L \rightarrow 0$ as $T \rightarrow T_{c}$.
The figure shows the temperature dependence of $L$ for water. The observed linear variation with
 negative gradient is consistent with (14).
[Figure courtesy of S.J. Blundell \& K.M. Blundell, Concepts in Thermal Physics, (OUP, 2006)]

